SYNTHESIS OF HYDROGEN PEROXIDE

Janak Kafle Chemistry 671

Introduction

- Oxidation
 - Functionalize molecules (selective or partial oxidation)
 - Remove pollutant (complete oxidation)

• Oxidizing Agents

- Oxygen gas
- Other oxidants (Sodium perborate, metallic peroxide etc.)
- Hydrogen peroxide

• Problems with oxygen gas

- Triplet ground state(in oxygen)
- Organic substrate (singlet ground state)
- Problems with other oxidants
 - Separation, poor atom efficiency, polluting
- Hydrogen peroxide

 $H_2S + H_2O_2 ----> S + 2H_2O$

Demand for hydrogen peroxide

• Current market of H₂O₂

- Three million metric tons per year
- As bleaching agent
- As cosmetics, disinfectants
- Chemical synthesis

In synthetic process

- Propylene oxide (PO) –polyurethanes
- Annual Production of PO is >six million metric tons
- Market of PO is increasing by 4-5% per year
- Presently PO is produced by oxidation of propene by organic peroxide

$\rm C_3H_6 + organic \ peroxide \rightarrow C_3H_6O$

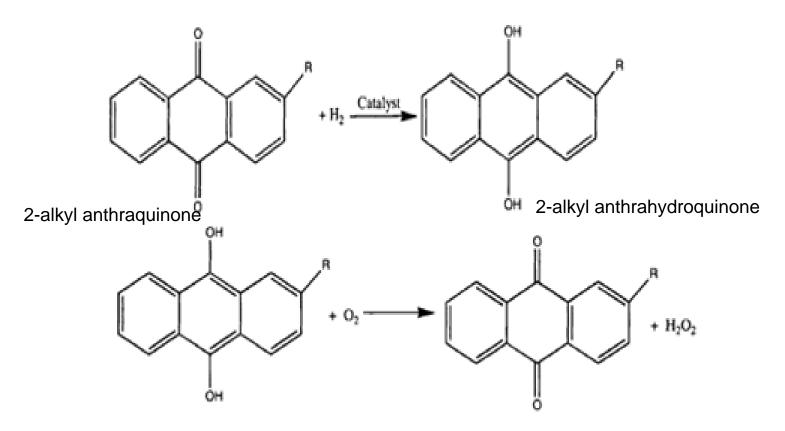
 Major PO producing company are designing a plant that produces 250,000 Metric tons/year of PO

- Needs 180,000 Metric tons of H_2O_2

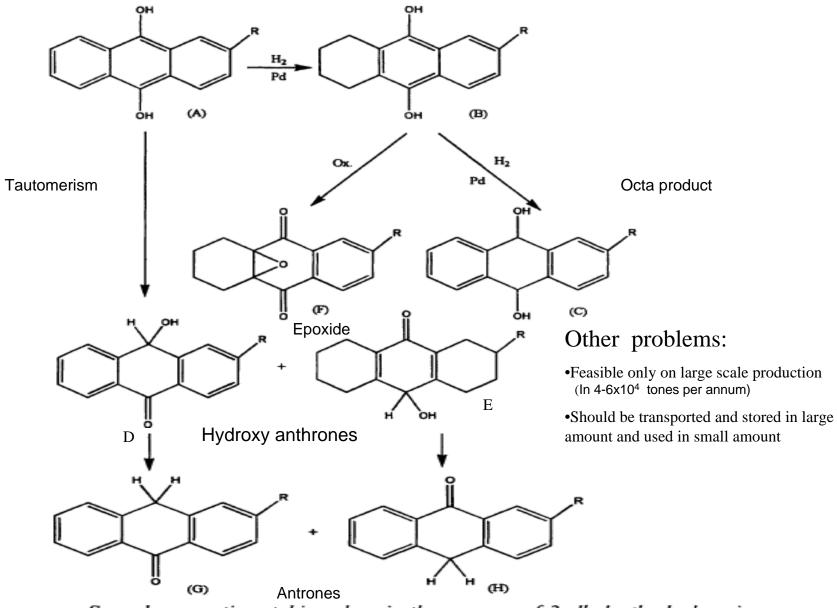
http://www.degussa.com/

Synthesis

• Is synthesis process green?



Synthesis of hydrogen peroxide from Anthraquinone



Secondary reactions taking place in the presence of 2-alkylanthrahydroquinones.

• Direct synthesis

Two reasons

1.Green2.Small scale production

 $H_2+O_2 \xrightarrow{Pt-group metals} H_2O_2$

Hydrogen and oxygen both are environmentally friendly reagents/No waste/very cost effective

Historical overview of direct synthesis

- Dr.Hugo Henkel and Dr. Walter Weber June 16,1913 filed a patent for direct combination of H_2 and O_2 to give H_2O_2
- Process claimed:
 - Porous pipe is impregnated with catalyst (**Pd**, Pt or Ni)
 - The pipe is placed under the water in a vessel under excessive pressure of oxygen (so the oxygen is in contact with out side of the pipe)
 - In to the interior of the pipe ,gaseous H_2 is forced ,the reaction occurs and hydrogen peroxide is produced.
- Pospelova,Kobozev,Eremin(1961)
 - Pd black,0.001N KCN,0.1 N H_2SO_4 ,20% H_2 initial yield 80 %

Problems with direct hydrogen peroxide synthesis

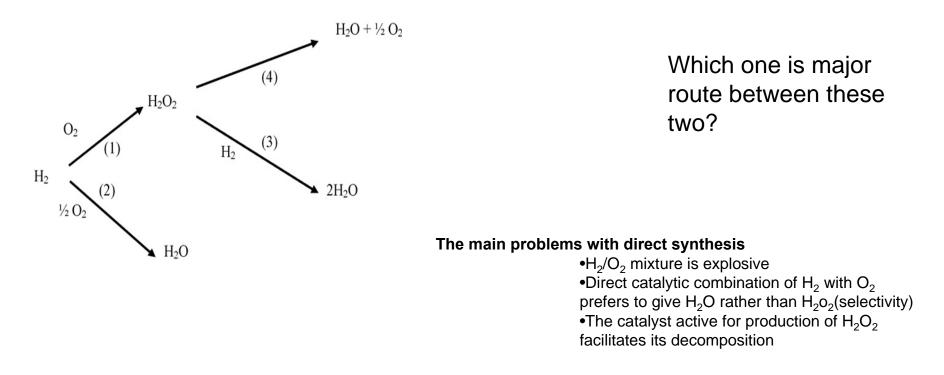
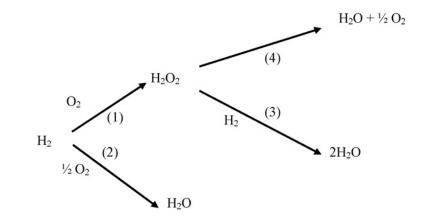


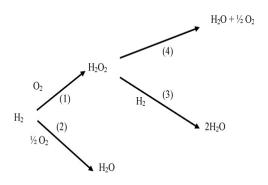
Fig. Various reactions during direct synthesis of hydrogen peroxide

• The favorable conditions

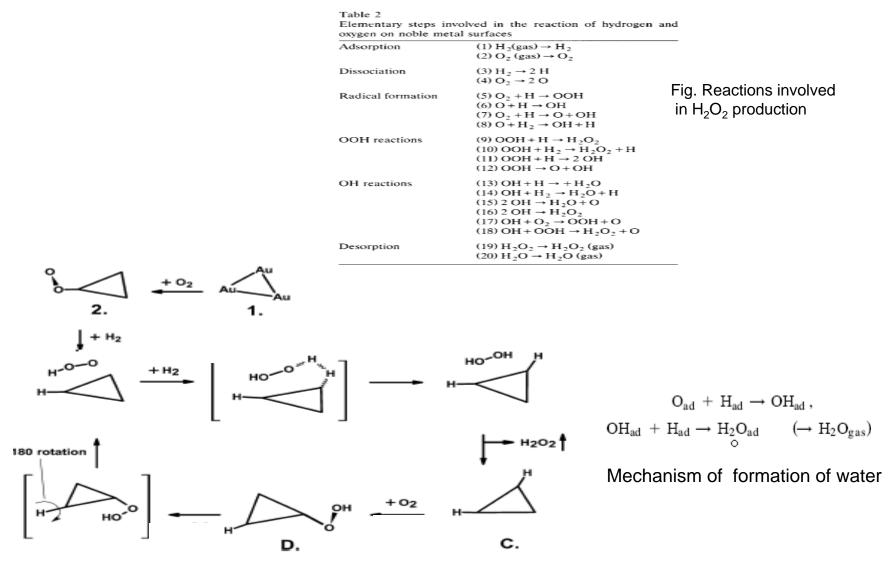
- Lower temperature
- Short reaction time
- High pressure
- Additive
- Catalyst



- Catalysts
 - Au, Ag, Pd, Au-Pd, Pd-Pt,
- Promoters
 - Acids
 - Bromide ions (NaBr)
- Role of acids
 - H_2O_2 is more stable in acidic condition. When [H⁺] is sufficient in the reaction medium ,rxn 3 is suppressed
- Role of bromide ions
 - Small amount of bromide improves selectivity of H_2O_2
 - More bromide reduces the concentration of H_2O_2 severely
- Reasons: Br⁻ is poison for Pd catalyst
 - Block very active water producing sites
 - (Poison the catalytic sites active in breaking O-O bond)
 - At more concentration it destroys the catalyst



Mechanisms of synthesis of hydrogen peroxide



Mechanism of formation of H_2O_2

Definitions

- Conversion=(moles hydrogen consumed/moles hydrogen fed)x100%
- Selectivity= [H₂O₂]/ [H₂O₂] +[H₂O]x100% =moles of H₂O₂ produced/moles of hydrogen consumedX100%
- Yield=Moles H₂O₂ produced/moles H₂ fedx100
- Productivity =grams of H₂O₂ produced /grams Pd /pt xhr

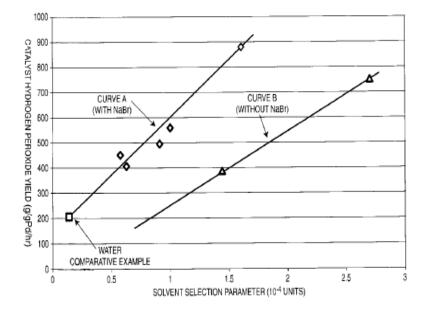
•The concentration of H_2O_2 is determined by iodometric titration/or titration with cerium sulfate or potassium permanganate

•The concentration of H_2O is determined by Karl-Fischer titration method

Solvent system used

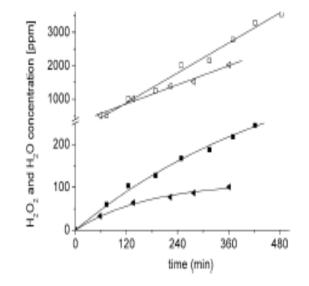
- Methanol is better than water
- Solvent selection parameter (SSP)
- Solvent selection
 - Solvent selection parameter (ssp)= $\sum (w_i \times s_i)$
 - w_i=weight fraction of solvent component *i* in liquid reaction mixture
 - s_i = solubility of H₂ in pure component *i* expressed in mole fraction at 25 °c and 1 atm
- As ssp increases H_2O_2 production increases
- Should have one phase, yield is high
- NaBr 3ppm to 200 ppm by wt of liq.rxn medium.

Effect of Solvent and Br-



1.Solvent selection parameter VS. Hydrogen peroxide yield

1.United States Patent 6576214



2 Fig. 6. Effect of the Br⁻ concentration on the catalytic activity of TCM2. Squares, 6 ppm Br⁻; triangles, 60 ppm Br⁻ (filled symbols, H₂O₂ concentration; open symbols, H₂O concentration).

2.S. Melada et al. / Journal of Catalysis 237 (2006) 213-219

			Effect of I	iquid Solve.	nt on Hyd	rogen Peroxid	e Synthesis			
Example Number	Liquid Mixture	Catalyst to liquid ratio	H ₂ Solubility in Solvent 1 atm 25 C. 10 ⁻⁴ mole fraction	H ₂ Solubility in Water 1 atm 25 C. 10 ⁻⁴ mole fraction	Weight fraction solvent	Solvent Selection Parameter Weight Average H ₂ Solubility 10 ⁻⁴ units	H ₂ in Feed (vol. %)	H2 Conversion (%)	H ₂ O ₂ Concentration (wt %)	H2O2 Yield (g/gPd/h)
				Com	parative E	xample				
1	Water	1/100		0.14 Curve A l	0 Examples	0.14 (with NaBr)	3	24.3	2.9	207
2	Methanol/Water	1/300	1.6	0.14	0.3	0.578	3	22	2.1	450
3	Acetonitrile/Water	1/300	1.76	0.14	0.3	0.626	3	18.9	1.9	407
4	Isopropanol/Water	1/300	2.7	0.14	0.3	0.908	3	19.8	2.3	493
5	Acetone/Water	1/300	3	0.14	0.3	0.998	3	61.1	2.6	557
6	Methanol	1/300	1.6	0.14	1	1.6	3	85.2	4.1	879
				Curve B E	xamples (v	without NaBr)	-			
7	DMF	1/300	1.44	0.14	1	1.44	3	64.4	1.8	385
8	Isopropanol	1/300	2.7	0.14	1	2.7	3	82.4	3.5	750
				0	ther Exam	ples				
9	Hexane/Water *	1/300	6.6	0.14	0.3	2.078	3	79	0	0
10	Formaldehyde/Water	1/300	?	0.14	0.3	?	3	11.8	0.3	64

1.United States Patent 6576214

Effect of solvent in production of hydrogen peroxide

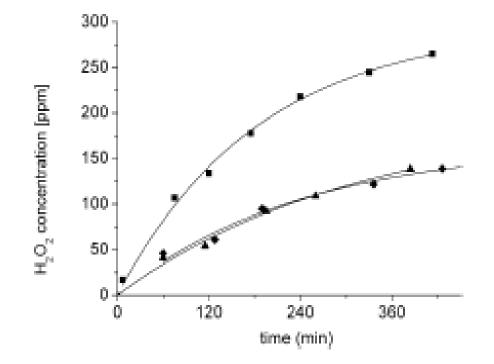


Fig. 3. H₂O₂ concentration profiles in different reaction media for TCM1.
■, 100% methanol; ◆, 100% water; ▲, 50% water and 50% methanol.

• The usefulness of solvent other than water

- Most oxidation process involving H₂O₂ are carried out in organic solvent
- Hydrogen and oxygen solubilities are higher in organic solvent than in water
- Dry organic media helps to measure the produced water and measure the catalytic activity and selectivity.

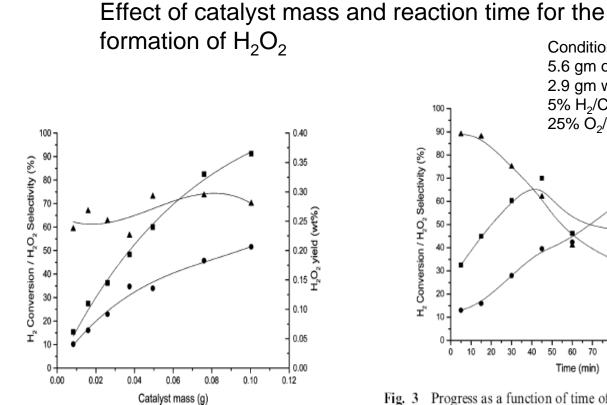


Fig. 2 Effect of catalyst mass on production of H₂O₂ using 0.6 wt.% Pd/sulfonated carbon, $\bullet = H_2$ conversion, $\blacktriangle = H_2O_2$ selectivity, $\blacksquare =$ H₂O₂ yield.

Fig. 3 Progress as a function of time of the reaction between H₂ and O_2 using 0.6 wt.% Pd/sulfonated carbon, $\bullet = H_2$ conversion, $\blacktriangle =$ H_2O_2 selectivity, $\blacksquare = H_2O_2$ yield.

Time (min)

40 50 60 70 80 90

Conditions:

 $25\% \bar{O}_{2}/C\bar{O}_{2}$

5.6 gm of MeOH 2.9 gm water 5% H₂/CO₂ and

0.40

0.35

0.30

0.25

0.20

0.15

0.10

0.05

0.00

100 110 120

H₂O₂ yield (wt%)

London Philip et.al. Direct synthesis of hydrogen peroxide from H₂ and O₂ using Pd and Au catalysts, Phys. Chem. Chem. Phys., 2003, 5, 1917-1923

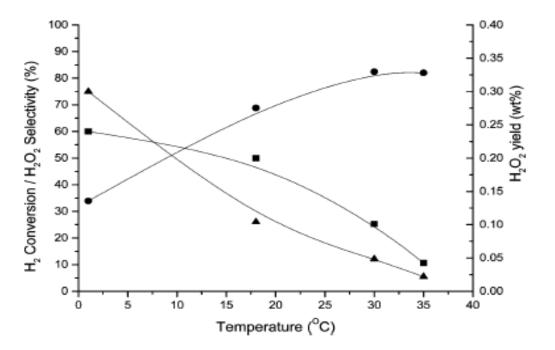


Fig. 4 Influence of temperature on H_2O_2 production using 0.6 wt.% Pd/sulfonated carbon $\bullet = H_2$ conversion, $\blacktriangle = H_2O_2$ selectivity, $\blacksquare = H_2O_2$ yield.

Philip Landon et al. Phys. Chem. Chem. Phys., 2003, 5, 1917–1923

Bimetallic catalyst

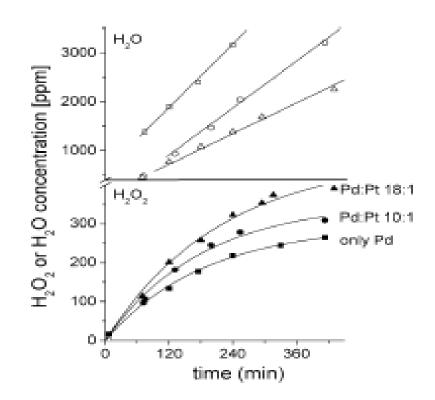
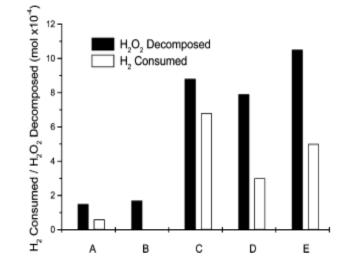


Fig. 7. Catalytic performance of bimetallic samples (TCM3 and TCM4) compared to a monometallic sample (TCM1). Filled symbols, H₂O₂ concentration open symbols, H₂O concentration.

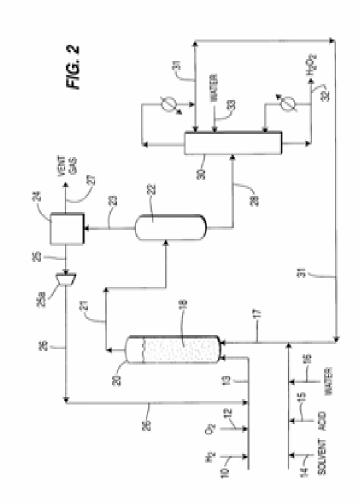
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Studies on possible decomposition route of hydrogen peroxide



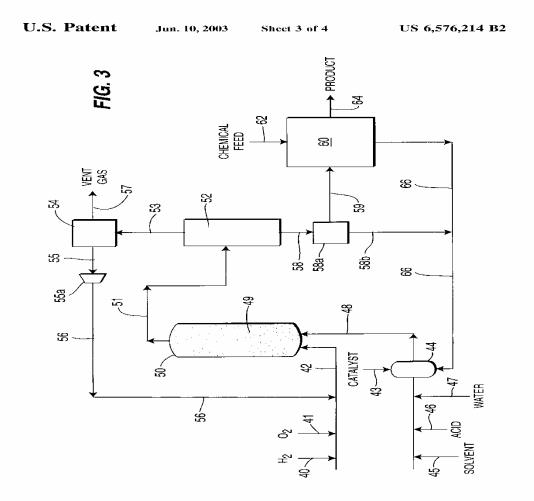
2 H₂O reaction 4 $\Delta H = -211.5 \text{ kJ mol}^{-1}$ + H₂ H₂O₂ reaction 1 ∆H = -135.8 kJ mol⁻¹ reaction 3 + 02 ∆H = -105.8 kJ mol⁻¹ H₂O + 0.5 O₂ H_2 + 0.5 O₂ reaction 2 $\Delta H = -241.6 \text{ kJ mol}^{-1}$ H_2O

Fig. 6 Decomposition of H_2O_2 under different experimental conditions using 0.6 wt.% Pd/sulfonated carbon, (A) = no catalyst, H_2 , 1°C, (B) = catalyst, O_2 , 1°C, (C) = catalyst, H_2 , 1°C, (D) = catalyst, H_2 , HBr (1.8 × 10⁻⁵ mol l⁻¹), 1°C, (E) = catalyst, H_2 , HBr (1.8 × 10⁻⁵ mol l⁻¹), 17°C, 3.7 MPa.

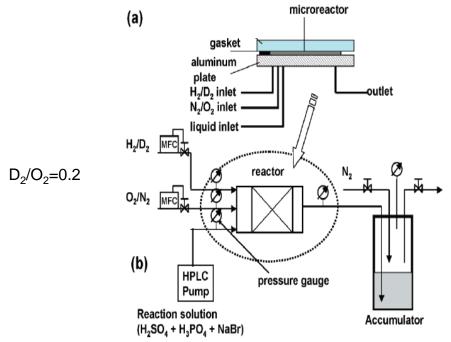


Direct synthesis of hydrogen peroxide

United States Patent 6576214



Direct synthesis of Hydrogen peroxide combined with organic synthesis



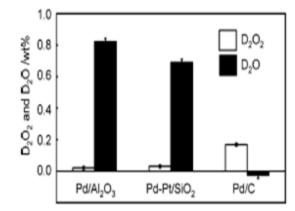
re 3. Hydrogen peroxide synthesis setup: (a) microreactor setup and (b) total system for direct synthesis of hydrogen peroxide.

$$H_2O_2$$
 produced
=0.2 wt%
 D_2 conversion =3 %

Selectivity is nearly 100 % Rate of production -first order in hydrogen partial pressure

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Figure 6. Comparison of formation of peroxide (open box) and water (filled box) on different catalyst supports, Pd/Al₂O₃ (13.5 mg), Pd-Pt/SiO₂ (29.0 mg), and Pd/C (15.6 mg). Conditions were as follows: deuterium flow rate 1.0 sccm, oxygen flow rate 4.0 sccm, and liquid (reaction solution flow rate 0.1 mL min⁻¹.

T=293K,P=2 MPa,0.05N H₂SO₄,H₃PO₄=0.015N,NaBr=5.1X 10⁻⁴ mol L-1

SCCM=standard cubic centimeter per minute

Conclusions:

- Direct synthesis of H_2O_2 from hydrogen and oxygen is convenient than anthraquinone process
- Pd/gold or Pd/Pt catalyst is better than single metal
- Short reaction time, high pressure and low temperature are favorable conditions
- There is possibility of making portable hydrgen peroxide synthesis device for small scale production
- Methanol/water mixture is good solvent system,NaBr is good additive and presence of acid are necessary conditions for maximizing the selectivity of hydrogen peroxide synthesis

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